



# Direct numerical simulation of the multispecies hypersonic boundary layers: Effect of gas-surface interaction on wall heating

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# Abstract

Planetary entry environment of hypersonic vehicles presents the extreme effects of high-temperature real-gas. Aeroshell of spacecraft heat shields are made of ablative materials in order to survive such high-energy environments. Ablation can impact surface heating via injecting pyrolysis gas into the boundary layer, thus prompt a strong interaction between the surface ablative materials and the boundary layer flow. By means of direction numerical simulation, the current study examines the effect of blowing at the wall on the aeroheating within the boundary layer subject to the thermochemical effects of vibrational excitation and dissociation of air mixture in hypersonic chemically reacting flows.

Keywords: blowing effect, aeroheating, hypersonic boundary layers, ablation

# Nomenclature

### Latin

- A wavemode amplitude
- to out-gassing
- $A_{\text{tot}}$  total surface area of the boundary layer
- $C_f$  skin friction
- $\vec{C}_H$  film coefficient or Stanton number for heat Greek transfer
- $C_M$  Stanton number for mass transfer
- M Mach number
- $\dot{m}$  mass flow rate per unit area
- $Re_{\theta}$  momentum thickness Reynolds number
- q heat flux
- $\dot{s}$  surface recession rate
- t time
- T temperature
- u instantaneous streamwise velocity
- U mean velocity
- v instantaneous normal velocity

- w instantaneous spanwise velocity
- x streamwise direction
- $A_{q}$  surface area of the boundary layer exposed y normal direction w.r.t the boundary layer surface
  - Y mass fraction of species
  - z -spanwise direction

  - $\beta$  spanwise wavenumber
  - $\delta^*$  boundary layer displacement thickness
  - $\rho$  density
  - $\tau$  shear stress
  - $\omega$  wavemode frequency
  - Subscripts
  - ca char ablation
  - e boundary-layer leading edge
  - g pyrolysis gas
  - s species
  - w wall
  - $\infty$  freestream

# 1. Introduction

Extreme environment of the hypersonic regime during planetary entry flights induces great challenges on the assessment of surface aeroheating and aerothermal prediction of boundary layers, leading to conservatism in the design of Thermal Protection System (TPS) of entry vehicles and spacecraft heat shields. Using ablative TPS materials via pyrolysis phenomenon is the only viable choice to mitigate extreme convective and radiative heat generated in high-enthalpy environments. Ablative materials as

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porous reactive materials containing several layers of solid phases and a single gas phase impose significant difficulties to determine the surface conditions of the boundary-layer flows of the ablative heat shield of the TPS of spacecrafts. As the surface is heated while the vehicle is traveling at hypersonic speed, the original composite material of the ablative TPS pyrolyzes, resulting in blowing gases through a porous residue. As an endothermic reaction, pyrolysis creates a strong coupling between the boundary layer flow and the transient heat conduction within the ablative material [1]. Modeling gas-surface interaction between the ablative material and boundary layer flow is one of the major issues in designing TPS. Ablation can affect the gas-surface interaction via three routes of (i) injecting pyrolysis gases and/or out-gassing of other ablation subproducts to the boundary layer, (ii) modifying the surface roughness due to the irregular pyrolysis, and (iii) altering the surface heat transfer due to the material-flow chemical reactions [2]. The role of each route on the gas-surface interaction can vary depending on the trajectory of entry flight. The comparable effects of these three routes on the boundary-layer flow and consequently surface aeroheating have not been understood yet. Determining the heat transfer coefficient and thermal response of ablative materials to high-enthalpy flows remains a challenge for the hypersonic vehicle design community.

Injecting gas into the boundary layer, as a means of reducing wall heat flux in hypersonic boundary layers has been already used in the transpiration cooling [3]. In agreement with the previous experiments, numerical investigations of transpiration cooling by injecting freestream gas into the low-speed flows at Mach 0.2 [4] and supersonic flows at Mach 2.67 [5] over flat plates demonstrate a reduction in skin friction and Stanton numbers as blowing increases. During planetary entry, the vibrational energy of atmospheric molecules are excited and chemical reactions are generated in the shock layers. By incorporating vibrational excitation and dissociation in hypersonic laminar boundary layers [6], the numerical simulation of temporally-developing hypersonic boundary layers [7] and spatially-developing hypersonic boundary layer [8] examine the thermochemical effects on boundary layer development which is previously studied only by the linear stability theory [9]. Over the last decades, there have been several numerical and experimental studies investigating the role of blowing or out-gassing on the surface heating of the boundary layers. Viscous shock layer calculation of the stagnation-point heat transfer in laminar flows over hyperboloids indicates that blowing equilibrium air into the reacting air can dramatically reduce the surface heat transfer rates.

Although measurements of the surface heat flux in high-speed boundary layers subject to the wall outgassing demonstrate the reduction of heat transfer rate, the underlying physical mechanism of mass injection-induced boundary layer laminar-turbulent transition and surface aeroheating in high-enthalpy flows are still unclear and remain a subject of active research. Using laminar hypothesis to simulate the flow field results in disagreement with surface aeroheating rate measurements of hypersonic vehicles [10, 11]. On the other hand, fully turbulent simulations of hypersonic flows over blunt bodies over-predict the surface heat flux in the upstream regions [12, 13]. Most stability analyses of hypersonic boundary layer consider the idealized scenarios of homogeneous blowing and calorically prefect gas with no chemical reaction [14-16], while a recent review by Candler [1] shows that chemical reaction and vibrational energy can have an important effect on the instability growth leading to the boundarylayer transition and surface heating. Empirical methods or engineering correlations are still being used as a set of practical tools to predict heat transfer rates and skin friction in high-speed flows. Among these correlations, in absence of a transition model, most designs of entry vehicles still follow some laminar solutions as a lower bound and turbulent correlations such as the van Driest's as an upper bound [17]. These correlations tend to over-predict heat transfer coefficients or Stanton number on cold walls ( $T_w/T_\infty$  <0.1) and under-predict them otherwise. Over-prediction of nose surface recession of the ablative heat shield of the Galileo probe has been attributed to a high level of inaccuracy in calculating the thermochemical state of the flow field [18], and thus failure of the heating-ablating analysis tools [19]. On the heat shield of the entry vehicles, aeroheating uncertainties are more than 50% mainly due to the early boundary-layer transition to turbulence, surface chemistry, and ablation-induced roughness. A primary source of these uncertainties is a lack of relevant flight data in order to improve model validations. A small amount of TPS performance data was obtained from the NASA missions by Pathfinder and MSL entry vehicles in the hypersonic and supersonic regimes. Generally speaking, there is a scarcity in direct measurements of aeroheating, aerodynamics, and environment atmosphere. To improve our understanding of aeroheating and TPS performance uncertainties, we believe that simulating the hypersonic boundary layer subject to ablation or to any single effect of ablation can be extremely helpful in a parallel effort to the flight measurement or experimental campaigns in Arc jet facilities.

The primary aim of this study is to advance our understanding of surface aeroheating by characterizing the gas-surface interaction, in particular the effect of surface blowing on the flow field. We investigate the blowing effect on surface heating in a spatially developing hypersonic boundary layer subject to the thermochemical effects of vibrational excitation and dissociation of multi-species gas mixture. The objective of this work is to understand the underlying physical mechanisms of convective-blockage effects by ablation-induced blowing on the aeroheating of a hypersonic boundary-layer flow. Toward developing an engineering-level analysis tool to correlate the experimental data of heating with surface blowing, we need to obtain a sound level of fundamental understanding of the effects of mass transfer on aeroheating. As a first step of modeling gas-surface interactions on an ablative heat shield, we aim to scale the heat transfer coefficient with an appropriate blowing parameter in the absence of surface roughness. In §2 different parameterizations of blowing rate and injection-induced diffusivity are discussed while briefly introducing gas-surface interactions and initialization are presented in §3, followed by results and discussion in §4 and finally we close by summary and future outlook in §5.

### 2. Theoretical background

For a mixture of ideal gases of a chemically reacting flow, we solve the the conservation of mass species, compressible Navier-Stokes, and energy equations, expressed in a vector form in a Cartesian coordinate given by:

$$\partial_t \mathbf{C} + \partial_x \left[ \mathbf{F}(\mathbf{C}) + \mathbf{F}_v(\mathbf{C}) + \partial_y \left[ \mathbf{G}(\mathbf{C}) + \mathbf{G}_v(\mathbf{C}) \right] + \partial_z \left[ \mathbf{H}(\mathbf{C}) + \mathbf{H}_v(\mathbf{C}) \right] \right] = \dot{s} \tag{1}$$

where the vector of conserved variables is  $\mathbf{C} = [\rho_1, \rho_2..., \rho_{N_s}, \rho u, \rho v, \rho w, \rho w]_0]^T$ . The partial density of species *i* is defined by  $\rho_i = \rho Y_i$  with  $\rho$  the density of N<sub>s</sub>-species mixture and  $Y_i$  the mass fraction of species *i*. **F**, **G** and **H** are Euler fluxes of the conserved variable vector **C** in the streamwise (x), normal (y), and spanwise (z) direction, respectively.  $\mathbf{F}_v$ ,  $\mathbf{G}_v$  and  $\mathbf{H}_v$  are diffusive fluxes of the conserved variables [20]. Since we here examine the hypersonic flows at high-Reynolds number, the second order central finite-difference scheme is used to evaluate the diffusive fluxes. While the Euler fluxes are evaluated using the sixth-order Targeted essentially non-oscillatory (TENO) scheme scheme. The source term  $\dot{s}$ , the RHS of Eq. 1 presents the chemical rate of mass production of species *i* per unit volume while considering both forward and backward reaction rates. Modeling ablative surfaces requires consideration of the mass flow rate into the boundary layer as well as a right modeling of  $\dot{s}$ . In a multispecies hypersonic boundary layer with not sufficiently small stagnation temperature, the gas mixture cannot be treated as calorically perfect gas as thermochemical effects are important. In this study we assume the dissociating air mixture subject to non-equilibrium effects and use Wilke's rule to evaluate dynamic viscosity of the air mixture.

#### 2.1. Non-dimensionalization and scaling of blowing

Blowing or out-gassing rates can be characterized by a non-dimensional parameter differently depending on various parameters such as the geometry of the boundary layer or the shape of surface roughness, to name a few. Early experimental study of the laminar boundary-layer flow of certain binary gas mixtures [21] characterizes blowing or injection rate at the wall by a single non-dimensional parameter defined as:

$$F_w = \frac{\rho_w v_w}{\rho_\infty u_\infty},\tag{2}$$

where  $\rho_w$  and  $v_w$  are density and normal velocity of the blown gas at the wall, respectively. Density and velocity of the inviscid freestream are denoted by  $\rho_\infty$  and  $u_\infty$ , respectively. With a minimal error, one can replace the freestream value in Eq.(2) with the mass flow rate per unit area at the boundary layer edge ( $\rho_e u_e$ ), however at the cost of determining the correct location of the boundary layer edge. To include the non-uniform distribution of gas injection along the heat-shield surface and the porosity of the surface,  $F_w$  can be modified by the base area of blowing and cross-sectional area of the porous section [22]. Since the distribution of blowing may not be uniform during pyrolysis, therefore the areaaveraged blowing parameter can be modified as:  $F_{w,a} = (\rho_{\infty} u_{\infty} A_{tot})^{-1} \int_{0}^{A_g} (\rho_w v_w) dA$ , where  $A_{tot}$  is the total surface area of the boundary layer and  $A_g$  is surface areas that pyrolysis gas is blown from. Such a scaling is more appropriate for flows over flat plates or blunt bodies at zero Angle of Attack (AOA), where classical inflection-point instability is the major player. While three-dimensional flows over the bodies at non-zero AOA can introduce an additional instability such as cross-flow instability [23].

To include the influence of blowing on aeroheating, film coefficient  $C_H$  of the non-blowing wall can be used to characterize a non-dimensional blowing parameter defined as [24]:

$$F_w^* = \frac{\rho_w v_w}{\rho_e u_e C_{H_o}},\tag{3}$$

where  $C_{H_o} = q_w/(\rho_e U_e C_p \Delta T)$  is the Stanton number for heat transfer or film coefficient of the nonblowing wall. Note that since  $F_w^*$  characterizes blowing locally as opposed to the averaged notion of  $F_{w,a}$ , it can give us the flexibility of investigating aeroheating of the stagnation-point region or any locations of interest that temperature or heat flux measurements are available. Then we can compare the aeroheating of these regions against the one of the same locations but with no blowing.

Finally, in some efforts of coupling between material response analysis and aerothermal calculation of the boundary layer, blowing can be scaled by the mass transfer coefficient, where  $C_{H_o}$  in Eq.(3) is replaced by  $C_M$ . That leads to a new non-dimensionless parameter characterizing blowing rates at the wall defined as [25]:

$$B' = \frac{\dot{m}_{tot}}{\rho_e u_e C_M},\tag{4}$$

where  $\dot{m}_{tot} = \dot{m}_g + \dot{m}_{ca}$  is the mass-flow rate (per unit area) of the total injected gas in which the mass-flow rate of the pyrolysis gas and char ablation gas are denoted by  $\dot{m}_g$  and  $\dot{m}_{ca}$ , respectively. The Stanton number for mass transfer is denoted by  $C_M = \dot{m}_s / [\rho_e u_e (Y_{s_e} - Y_{s_w}]]$ , where  $\dot{m}_s$  is the mass-flow rate of species s. The mass fraction of species s at the boundary-layer edge and the wall are denoted by  $Y_{s_e}$  and  $Y_{s_w}$ , respectively. In the present study, we use the scaling notion of Eq.(3) to non-dimensionalize the velocity of gas blowing into the boundary layer to explicate the relationship between surface out-gassing and aeroheating in the hypersonic boundary layers.

#### 2.2. Gas-surface interaction

To compute the aerothermal environment of the atmospheric entry flights, surface heat flux is inferred from the temperature measurements and thermal response assumptions, where the latter is either empirically modeled through calibration or explicitly modeled via a mathematical analysis. In this case, surface heating must be inferred from the actual sensor measurements of the embedded thermocouples inside the ablative heatshield of the TPS of a spacecraft. On an ablator, the location of boundary varies due to recession and chemical interactions. The recession model is used to estimate this surface location. Considering the ablator as a solid material composite of multiple components and pyrolysis zone as shown in Fig. 1, surface temperature can be obtained by solving the energy transport equation from the perspective of the gas-surface interaction. By conducting the surface energy balance, the storage rate of sensible heat evaluated at a recessed coordinate ( $y_r$ ) is given by:

$$\rho c_p \frac{\partial T}{\partial t}|_{y_r} = \frac{1}{A_{tot}} \frac{\partial}{\partial y_r} \left( k A_{tot} \frac{\partial T}{\partial y_r} - q_{rad} \right) + \frac{\dot{m}_g}{A_g} \frac{\partial h_g}{\partial y_r} + (h_g - \bar{h}) \frac{\partial \rho}{\partial t}|_y + \dot{s} \rho c_p \frac{\partial T}{\partial y_r}$$
(5)

where y is the stationary coordinate system in which the virgin material resides initially and  $y_r$  is the coordinate system moving with the recession surface. The local cross-section of the material exposed to the pyrolysis gas mass-flow rate  $(\dot{m}_g)$  and enthlapy  $(h_g)$  is denoted by  $A_g$  that is heated via conduction and pyrolysis gas convection. The surface recession rate is denoted by  $\dot{s}$ , enthalpy by h and temperature by T. We here assume that partially pyrolyzed material is a simple mixture of pure virgin material and pure char. Therefore density of the partially pyrolyzed material is denoted by  $\rho$  such that  $\rho_c < \rho < \rho_v$ , where the virgin and char material properties are denoted by  $(\cdot)_v$  and  $(\cdot)_c$ , respectively. The mass fraction of the virgin material in a mixture of virgin material and char denoted by  $r_v$  is defined

by  $r_v = (1 - \frac{\rho_c}{\rho})/(1 - \frac{\rho_c}{\rho_v})$ . Similar to density, all other material properties of a mixture used in Eq. (5) such as specific heat coefficient ( $c_p$ ) and thermal conductivity (k) are weighted following the mixture rule,  $(\cdot) = (\cdot)_v (\cdot)_{p,v} + (1 - r_v) (\cdot)_{p,c}$ .





Fig 1. Surface energy balance in the boundary layer of the ablative material

As the material is heated, one (or more) component(s) of virgin material pyrolyzes and produces char and pyrolysis gas, yielding out-gassing or injecting mass which percolates away from the pyrolysis zone and goes through pores of charred zone and finds its way to the boundary-layer flow. Besides injecting mass, there is also heat flux into the boundary layer. The first term on the RHS of Eq. (5) is the net rate of conductive and radiative heat flux. The second term on the RHS is the rate of energy convected by pyrolysis gas, the third term is consumption rate of the pyrolysis energy, and finally the last term o the RHS of the Eq. (5) is rate of convective (sensible) heat flux due to recession. The quantity  $\bar{h}$  in Eq. (5) is the density weighted enthalpy difference between the virgin material and char defined by  $\bar{h} = \frac{\rho_v h_v - \rho_c h_c}{\rho_v - \rho_c}$ . The enthalpy of the pyrolysis gas is a function of the wall temperature, pressure and mass fraction:  $h_g = f(T_w, p_w, r_v)$  [2].

## 2.3. Boundary conditions

To consider the ablation process in the high-enthalpy hypersonic flow simulation, surface boundary conditions are tremendously more complicated than modeling the passive material or the more conventionally used no-slip boundary conditions. Here we assume a non-catalytic surface. The computational domain along the boundary conditions are shown in Fig. 2. Blowing or out-gassing boundary condi-





tion at the bottom wall is implemented by altering the normal component of velocity at the surface as schematically depicted in Fig. 2. Ablative materials are porous reactive materials containing several layers of solid phases and a single gas phase. Modeling mass and heat transfer from such materials to the boundary layers requires a coupling strategy incorporating the ablating surface energy balance and the aerothermal environment calculations. The main idea here is to solve the compressible Navier-Stokes equations, along with the continuity of each species, and the two-temperature model of energy transport equations. However to model the energy balance at the gas-surface interface, we need to calculate the heating influx from the environment into the boundary layer and cooling out-flux from the effective surface of the porous material to the boundary layer as illustrated in literature [26]. Therefore, it is necessary to locate the boundary-layer edge and to calculate boundary-layer parameters in a separate step.

The bottom wall (orange surface in Fig. 2) is assumed to be an isothermal wall boundary condition on temperature and no-slip on velocity. The constant cold temperature is  $T_w/T_e = 6.5$  close to the laminar adiabatic wall temperature or about 79 % of the stagnation temperature, where  $T_w$  and  $T_e$  are temperature at the wall and boundary layer edge, respectively. In the spanwise (z) direction, periodic boundary conditions are used whereas characteristic outflow boundary conditions are used on the top and downstream boundaries.

# 3. Numerical Method

To compute the flow field, we use an open-source code, the Hypersonics Task-based Research (HTR) solver [20] developed for DNS of hypersonic flows subject to aerothermo-chemical effects in structured grids, while including the finite-rate chemistry and thermal non-equilibrium. In order to handle the stiffness induced by vastly different time scales with efficiency and stability, the solver here employs two different time-advancement schemes: a third-order Runge–Kutta method when the chemical reactions are slow, and an operator-splitting method when chemical reactions are fast and the numerical integration becomes correspondingly stiff. For spatial discretization, a low-dissipation sixth-order TENO scheme is used as a compromise solution between low numerical dissipation and stable capture of shocks. The viscous terms are computed with second-order spatial accuracy with a central difference approach. Since the HTR solver is based on a multi-component transport formulation, we can incorporate variable specific heat capacities and transport coefficients along with a chemical-kinetic description for air dissociation. This formulation enables the investigation of phenomena induced by vibrational excitation of air molecules and their dissociation in hypersonic flows at high Reynolds numbers.

To accurately represent the high-enthalpy flows, modeling the gas transport properties is crucial. Here, the diffusion coefficients of the multi-component of the gas mixture are evaluated using the self-consistent effective binary diffusion model [27]. The mixture viscosity and thermal conductivity of multi-species gas are evaluated by using the kinetic-theory-based model and Yos approximate mixing rules [28]. To compute vibrational thermal conductivity, the standard expression with vibrational temperature gradients is used as since simulations with energy gradients tend to be unstable for the dissociated flow. The advantage of the HTR solver is in deployment of the GPU-based high-performance computation. In contrast to the traditional domain-decomposition methods in the parallel CFD solvers, the HTR solver is developed on the task-based environment provided by the versatile libraries of the programming language model of Legion [29]. Specifically designed for writing memory-hierarchy-agnostic programs, Legion is more efficient and less costly in memory-management operations compared to the conventional Message Passing Interface (MPI) structures.

For all simulations, the Reynolds number is based on inflow displacement thickness and freestream viscosity and freestream velocity:  $\text{Re}=\delta_0^*\rho_\infty u_\infty/\mu_\infty$  =3000, where  $\mu_\infty$  is dynamic viscosity and  $\rho_\infty$  density of freestream,  $\delta_0^*$  is the displacement thickness of the boundary layer at the inflow boundary condition located at  $x = x_0$ . This is the start of an undisturbed compressible laminar boundary layer, in which velocity and temperature profiles are imposed by self-similar solutions. Note that the origin of the streamwise coordinate x = 0 corresponds to the leading edge of the plate, which is not considered as  $x = x_0$  in these calculations. The power law  $\mu = \mu_{\text{ref}} (T/T_{\text{ref}})^{\sigma}$  is used to compute dynamic viscosity of the gas, where with  $\sigma = 0.7$ , and where  $\mu_{\text{ref}}$  is a reference value of viscosity evaluated at the reference temperature  $T_{\text{ref}}$ . Once  $c_p$  and  $\mu$  are calculated, the thermal conductivity in Eq. 5  $k = \text{Pr}/\mu c_p$  is evaluated by assuming a

constant value of the Prandtl number, Pr.

All lengths in the computational domain schematically shown in Fig. 2 are non-dimensionalized by  $\delta_0^*$  for the simulation. The domain is rectangular with uniform spacing in the spanwise (z) and streamwise (x) directions whereas a hyperbolic-tangent stretching is used in the wall-normal (y) direction in order to cluster cells near the wall. The stretching parameter of the distribution is determined by enforcing that the wall-normal size of the first grid element close to the wall. Therefore  $\Delta y^+ = 0.3$  which is normalized in viscous units measured at the exit domain boundary, while in the streamwise and spanwise directions are  $\Delta x^+ = 2.0$  and  $\Delta z^+ = 1.8$ , respectively. A summary of the domain size, number of grid points and resolution for all simulation scenarios can be found in Table 1.

Table 1. Summary of DNS computation setup with  $Re_{\theta,max}$ =2650, M=6 and  $T_w/T_e$  =6.5

$N_x$	$N_y$	$N_z$	$L_x$	$L_y$	$L_z$
4096	250	288	1000	75	$20\pi$

The distribution of the out-gassing velocity  $v_w$  is assumed to be uniform with the form of

$$v_w = f(x)\Sigma_i^2 A_i \sin(\omega_i t - \beta_i z)$$
  
where  $f(x) = \frac{1}{4x_s} \left[ \text{erf}\left(\frac{x + x_s}{\sigma\sqrt{2}}\right) - \text{erf}\left(\frac{x - x_s}{\sigma\sqrt{2}}\right) \right]$  (6)

where the function f(x) forces a Gaussian-like profile of perturbation in the streamwise (x) direction, with  $x_s = 15\delta_0^*$  and  $\sigma = 0.75\delta_0^*$  and  $\delta_0^*$  is the boundary layer displacement thickness at te inflow boundary condition. To achieve the oblique breakdown, we use two opposite modes parametrized by the wavemode amplitude of  $A = [0.05u_{\infty}, 0.05u_{\infty}]$ , the wavemode frequency of  $\omega = [0.9\delta_0^*/a_{\infty}, 0.9\delta_0^*/a_{\infty}]$ , and the spanwise wavenumber of  $\beta = [0.3/\delta_0^*, -0.3/\delta_0^*]$ , where  $a_{\infty}$  is speed of sound in the freestream. Freestream velocity  $u_{\infty}$  can be evaluated based on the freestream Mach number  $M_{\infty} = 6$  and  $T_{\infty}$ =450 K.

#### 4. Results & Discussion

Skin friction of the laminar boundary layer over the non-blowing surface is contrasted against boundary layer over the surface with the blowing parameter of  $F_w$ =0.005, depicted in Fig. 3. Comparing the case of the boundary layer over the non-blowing wall with the one for the blowing case in Figure 3 demonstrates the reduction skin friction since  $C_f = \tau_w/(1/2\rho_\infty u_\infty^2)$ , where  $\tau_w$  is the wall shear stress. Surface blowing introduces more mass momentum to the boundary layer, results in the suppression of the viscous force. However, the heat transfer per unit area  $q_w$  shown in Figure 4 (dashed lines) is inhibited by the surface blowing much more dramatically. This is the verification of what has been hypothesized earlier that injecting pyrolysis gas into the boundary layer reduces the heat transfer rate via *convective blockage effect* [30].

To understand how the out-gassing is modelled on the surface of the boundary layer, it's useful to monitor the evolution of the distribution of the density at the wall  $\rho_w$ . Fig. 5 (a) shows the time-averaged of  $\rho_w$  initially and in later time in Fig. 5 (b). The surface pressure (not shown here) also follows the same trend as the density at the wall shown in Fig. 5. Although initially density is uniform along the surface , due to the cooling effect of the injected gas, density and consequently pressure at the surface increases. We should not confuse the causation as it is important to note that the profile of cooling shown in Fig. 4 due to the increase of the density shown in Fig. 5 (b) as blowing rate increases.

The effect of out-gassing on the local characteristics of a boundary layer is examined in terms of the spanwise vorticity for three blowing rates as shown in Fig. 6. Except the growth of the boundary layer thickness, it seems that vorticity structures remain intact but that is not the cases as more gas is blown into the boundary layer. This is also evident from the density contour plots shown in Fig. 7. Also the laminar structure of the flow is disturbed as blowing rate increases (as shown Figure 7 (c), presumably the flow is triggered toward more transition regime, though not being achieved yet.



**Fig 3.** Spanwise- and time-averaged skin-friction coefficient,  $C_f$  at the wall as function of the normalized streamwise coordinate  $(x - x_0)/\delta_0^*$  for (a) the non-blowing case  $F_w$ =0 and (b) the case of out-gassing rate of  $F_w$ = 0.005.

Since the present simulations utilize a numerical method that does not use any filter nor requires any flux limiter, higher resolution across the boundary layer especially in the streamwise and normal directions has been implemented. Here, the blown gas has the same temperature as the surface temperature, therefor the pyrolysis gas enthalpy  $h_g$  in Eq. (5) is not accurately modelled yet. Also the injection gas has the same composition as the freestream gas, a binary air mixture of 79% $N_2$  and 21%  $O_2$ , which is in in chemical equilibrium at temperature  $T_{\infty}$  = 450 K and pressure  $P_{\infty}$  = 1 atm. The chemical equilibrium in the freestream is largely displaced toward the reactants and leads to a negligible dissociation degree. Zero wall-normal gradients are imposed for all species mass fractions at the wall. The inflow boundary conditions are obtained by solving the laminar, locally self-similar boundary-layer equations including species transport and chemical reactions. The more interesting question is how the results alter in case of injecting a foreign gas, also at the temperature that corresponds to the material response modeling the ablative material behavior at the surface.

#### 5. Summary

Ablation manifested by mass injection pushes the laminar boundary-layer edge away from the surface and shields the body from the high-temperature shock-layer gas. The response of the laminar boundary layer to surface blowing is an augmentation of density due to additional mass transfer and the reduction of viscosity at the wall which is primarily attributed to the cooling effect of surface blowing. Out-gassing has a minimal effect on the wall pressure in laminar boundary layers. To reduce uncertainty in calculation of the hypersonic boundary-layer flow field as well as to expand on the investigation of the effect of mass transfer on aerothermal heating, more sensitivity analyses implementing the local or point-wise injection velocity at the wall and also more computationally-demanding variations of in-depth properties are needed. Depending on which ablative material is used, the type and concentration of pyrolysis gas



**Fig 4.** Spanwise- and time-averaged normalized heat-flux,  $q_w/\rho_{\infty}u_{\infty}^3$  at the wall as function of the normalized streamwise coordinate  $(x - x_0)/\delta_0^*$  for (a) the non-blowing case  $F_w$ =0 and (b) the case of out-gassing rate of  $F_w$ = 0.005.



**Fig 5.** Spanwise- and time-averaged density at the wall along the normalized streamwise coordinate  $(x - x_0)/\delta_0^*$  for different blowing rates (a) initial condition (b) one flow-thorough-time

mixture vary. To provide a deeper understating of the physical mechanism underlying the effect of outgassing on aerothermal flow field, we indeed demand more experimental data in high-enthalpy boundary flows. This work is one step toward understanding the fluid-structure interaction via blowing effect on aeroheating at the extreme environment of hypersonic flight, though realizing high-fidelity simulations of the hypersonic flow environment is far from complete. Since hypersonic flight systems undergo various changes during flight over a large range of time scales, it is important to include relevant processes such



**Fig 6.** Contour plots of vorticity for (a) the non-blowing case  $F_w=0$ , (b) the case of out-gassing rate of  $F_w=0.005$  and (c) 0.015. For all three scenarios the vorticity at the distance of  $0.75L_x$  from the leading edge of the boundary layer is plotted.



**Fig 7.** Contour plots of density for (a) the non-blowing case, (b) the case of out-gassing of  $F_w$  0.005 and (c) 0.015 at 0.75 $L_x$ .

as roughness modification, material degradation, shape change, and recession.

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